

DOCTORAL DISSERTATION

STUDY OF CARBON STEEL CORROSION INHIBITION IN ACID MEDIUM

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SUMMARY

Acids are intensively used in different industrial technological processes : crude oil and gases extraction and processing, decapping of metallic pieces by oxides, industrial cleaning and other chemical and petrochemical operations. Also, on fractionary distillation of oil, due to salt hydrolysis, result acids with destructive effect on installations. In refineries, acid corrosion is an important and expensive aspect of activity, which causes production losses, inefficient processes, supplemental costs and for corrosion control compounds.

Using inhibitors is one of the most practical methods for anticorrosion protection, especially in acid media, from all methods and techniques, tried and used.

Inhibitors are compounds which controls, reduce or delay reactions between metal and environment, when are used in small amounts. The last aspect present economic interest. Between the studied categories of inhibitors, organic inhibitors presents a great interest for their effects on reducing corrosion processes in miscellaneous domains.

The corrosion inhibition efficiency by organic compounds, depends with layer structure and properties formed on the metallic surface, many of these organic compounds acting by adsorption on the metal surface.

The inhibition power by organic inhibitors, was analysed through many characteristics such as : molecular volume, molar mass, molecular structure, heteroatoms nature form molecule etc.

Organic compounds containing nitrogen and sulphur atoms, have a great interest in using as corrosion inhibitors for carbon steel, because they showed superior inhibition efficiencies to organic compounds only with nitrogen atoms, or only with sulphur atoms. Identification and evaluation of corrosion organic inhibitors of carbon steel in acid media, are important aspects to be solved practically, industrially and theoretically.

The aim of this study is to analyse the inhibition effect of two inhibitors in hydrochloric acid solution 2M :

- N-(2-hydroxy) tiosemicarbazide, HBTC and
- N-acetyl p-aminobenzene sulfonamide, APAS.

The hydrochloric acid solution was chosen, for intense use in miscellaneous domains and for his high aggressivity showed on carbon steel.

Behind the practical objectives, this study also wants a better understanding of processes that take place on the carbon steel surface in time of immersion in hydrochloric acid solution 2M, with different concentrations of HBTC or APAS.

For achievement of the study were used weight loss and potentiostatic measurements, rounded up with scanning electron microscopy (SEM) and Mössbauer spectrometry of carbon steel surface.

The working electrode, was made from carbon steel, with following composition (weight %):

| C | Si | Mn | Ni | Cr | Fe |
|-----|-------|-----|-----|-----|------|
| 0,1 | 0,035 | 0,4 | 0,3 | 0,3 | rest |

The study has 3 chapters and is based on a large volume of reference materials. In first chapter are systematized bibliographical dates of definition and corrosion categories, with development of electrochemical corrosion phenomenon for carbon steel. Are approached also essential elements for characterization of corrosion inhibitors, and in the end are shown dates about investigation in speciality literature of a carbon steel mixed type corrosion inhibitors, in different acid solutions, presentation finalized with conclusions about the mechanisms that produce carbon steel corrosion inhibition. This exposure about some of the best known mixed type corrosion inhibitors, was necessary for situation in the context of study theme.

In second chapter are described work methods, experimental and calculation sequencies, characteristic functions, mathematical judgements. Also are mentioned working standards, about some of activities in the study.

Chapter I and II together makes first part of study. The second part of the study is formed from chapter III, which contains research results about carbon steel corrosion inhibition in hydrochloric acid solution 2M, with different concentrations of organic compounds HBTC and APAS, obtained from weight loss and potentiostatic measurements, associated with scanning electron microscopy and surface Mössbauer spectrometry. (CEMS).

Chapter III begins with carbon steel surface characterization in hydrochloric acid solution 2M which will be used for comparison in next stages of experiment.

Weight loss and electrochemical conduct of carbon steel diluted in HCl 2M solution

The gravimetric measurements based on hydrogen volumetric determinations, had permitted calculation and representation of corrosion rate and corrosion penetration, according with the experiment temperatures.

In both situations the drawings do not present linear evolutions in the way that they start with induction corrosion periods, due the corrosion rates rise in value with the temperature, the most increased being at 45⁰C and especially at 55⁰C.

Using average values for corrosion rate from weight loss data, the representation of these values according with the temperature are exponential, fact which shows a fast and substantial development of the corrosion pending with temperature increase. The exponential equation is $y = 1,6974e^{0,0731x}$.

The same element is relieved from the penetration index I_p , which present a value (105,2 mm/year) at 55⁰C of aproximative 9 times higher compared with I_p value at 25⁰C (11,226 mm/year).

A linear variation is seen in the drawing representation of the formed hydrogen volumes during the temperature experiment. Here, as well, the experiment temperature increasing effect is obviously reflected at 45⁰C and especially at 55⁰C.

From the weight loss point of view is seen that carbon steel corrosion developing process in HCl 2M solution is maximal in the last third of the experiment period.

It comes up also that the steel carbon corrosion speed values, depend by the experiment period in which the weight loss measurements are done.

The activation energy values, graphical and analytical determined are about 59 KJ/mol.

For the electrochemical measurements it was used the potentiostatical method in a standard electrochemical cell with 3 electrodes. The main used electrode was the calomel-electrode, being used through a Luggin capilar. The measurements fulfilling source was a KEITHLEY 2420 3A SOURCE METER with data prelucreation computer.

For anode and cathode polarisation was done a set of five determinations at the room temperature, taking in consideration the most reproducible replicas.

It is seen high values for i_{cor} ($i_{cor} = 0,35 \text{ mA/cm}^2$), b_a ($b_a = 102 \text{ mV}$) which shows the carbon steel corrosion process in HCl solution 2M is intense also at surface as profound the metal mass.

The slope b_a with high value, shows that the steel carbon is very active and the anode desolving reaction is intense. The corroded carbon steel surface in solution of HCl 2M, examined on a electronic microscope VEGA TESCAN, is noticed by the intensity of the corrosion parts, alteration of the metallic texture, noticed and confirmed elements by the Mössbauer spectroscopic measurements. The doublet figures for the corroded item in HCl 2M, shows the presence of Fe^{3+} , α , β , γ - FeOOH and $\text{Fe}(\text{OH})_3$ compounds.

Carbon steel corrosion inhibition in HCl 2M solution, using as inhibitor HBTC, in different concentrations

In this sequence the will was to investigate the determined effects of different concentrations of HBTC in HCl 2M solution, regarding carbon steel corrosion inhibition. All measurements had been done at room temperature.

From the weight loss point of view, had been determined corrosion rates as gravimetric values k_g and penetration index I_p , as well in HCl 2M solution without inhibitor as in HCl 2M solution with HBTC having the concentrations : 0,1 mM; 0,2 mM; 0,3 mM; 0,4 mM.

The presence of HBTC in HCl 2M solution, determine the following decrease of the corrosion rate ($\text{g}\cdot\text{m}^{-2}\cdot\text{h}^{-1}$) :

- at $c = 0,1 \text{ mM}$, reduction is 45%;
- at $c = 0,2 \text{ mM}$, reduction is 53%;
- at $c = 0,3 \text{ mM}$, reduction is 65%;
- at $c = 0,4 \text{ mM}$, reduction is 75%.

Same differences can be observed also in the case of corrosion rate considered as corrosion penetration. Is clear the produced effect by the increasing of HBTC concentration in HCl 2M solution, over the decreasing of carbon steel corrosion speed and over the size values of the percentage inhibition efficiency from weight loss (at $c = 0,4 \text{ mM}$ HBTC, $P = 74,25\%$, and $P = 44,2\%$ at $c = 0,1 \text{ mM}$ HBTC).

From the graphical representation it is seen as well, the increasing of P values in the same time with the increasing of HBTC concentrations.

The inhibition effect of the carbon steel corrosion determined by the presence of HBTC in HCl 2M solution, is the result of HBTC molecules adsorption on the metal surface through the existing interaction between the couple of unparticipant electrons from the nitrogen and sulphur atoms, parts present in the lateral wing of the HBTC molecules and the metal.

It is possible to be formed on the carbon steel surface of some complexes by HBTC molecules (as ligand) and different steel metal cations, which are conducting a stable passive layer on the metal surface.

Adsorption is also confirmed by the increased value of the equilibrium constant (adsorption-desorption) $K = 5676 \text{ M}^{-1}\text{L}$ and adsorption enthalpy which is indicating a spontaneously adsorption process.

As in the previous sequence, the experimental figures drive to a Langmuir adsorption isotherm.

The carbon steel polarity curves for investigated HBTC concentrations, shows in comparison with the no inhibitor polarity curves, the action of HBTC as mixed inhibitor with stronger effect over the metal dissolving reaction. The same elements are noticed by the electrodynamic parameters values determined by Tafel straight lines.

Electrochemical percentage determined inhibition efficiency has close values to the weight loss one (at $c = 0,4 \text{ mM}$, $P_g = 74,25\%$ and $P_e = 73,3\%$).

Through electronic microscopy of the carbon steel surface samples, after corrosion in HCl 2M solution having $0,1 \text{ mM}$ HBTC; $0,2 \text{ mM}$ HBTC; $0,3 \text{ mM}$ HBTC; $0,4 \text{ mM}$ HBTC, it is noticed the existence of a thin film at the carbon steel surface and the reduction of the corrosion centers intensity.

The CEMS spectrum of the corroded sample in HCl 2M solution with HBTC, shows that the depth of the corroded surface is smaller due to the inhibitor presence. In the same respect, the corrosion process is considered slow down, being formed a superficial compound of Fe^{3+} , without any magnetic arrangement. Counting its relative area, this compound has a smaller thickness than the layer formed in the no inhibitor corrosion process.

Mössbauer parameters of the compound in this case, are not significantly different in comparison with the compounds found in the no inhibitor solution for the corroded sample. New parameters can be associated to other superficial compounds as ferrihydrates. It is well known that ferrihydrite is a forerunner for other demanded oxyhydroxides.

We consider that HBTC inhibitor act as an incipient "rust transformer" favouring formation of a "superficial closed layer". The inhibitor transform some constituents of rust into corrosion inhibiting oxide phases.

It was determined $3,33 \times 10^{-4} \text{ M}$ HBTC concentration as optimal concentration and in next study has been done detailed analysis for that inhibitor concentration.

Electrochemical and gravimetric behaviour of carbon steel in solution of HCl 2M consisting of $3,33 \times 10^{-4}$ M HBTC

The target is the investigation of the presence effect of $3,33 \times 10^{-4}$ M HBTC in HCl 2M solution towards carbon steel corrosion inhibition.

The operation part specific running was to use a single concentration of HBTC in the HCl 2M solution. The experiment was run at four temperatures, also in HCl 2M solution without inhibitor, as well as in HCl 2M solution with HBTC mentioned concentration.

The carbon steel corrosion rates revealed as weight loss values k_g , at the experiment temperatures, are seriously decreased in HCl 2M solution with HBTC, in comparison with solution without HBTC. The decrease is more pronounced at temperatures of 25°C and 35°C (7 times, and 4 times). At the temperatures of 45°C and 55°C the decreasing of the corrosion rates are quantitative smaller (3,5 times, and 2,65 times). It is obvious the inhibition effect of the carbon steel corrosion due to the presence of the HBTC, effect with a maximum value at 25°C.

According to the increasing of the temperature, the corrosion rates rise, the most important difference being between the corrosion rate at 55°C and 45°C obvious seen in the graphic and in the HCl 2M solution with $3,33 \times 10^{-4}$ M HBTC. This item is well seen in the graphical representations of the formed hydrogen volumes, penetration index I_p , corrosion inhibition coefficient C.

Corrosion average rates representations ($k_{g \text{ mediu}}$) of the carbon steel for the HCl 2M solution with or without inhibitor, have exponential form, having in the following order the equations :

1) $y = 1,6449e^{0,0736x}$ for the solution without inhibitor and

2) $y = 0,1153e^{0,1046x}$ for the solution with $3,33 \times 10^{-4}$ M HBTC.

The maximal values of the percentage inhibition efficiency are recorded at 25°C temperature, the average value being 85,78%. To the other temperatures the inhibition efficiency values are decreasing, the smallest being at temperature of 55°C (the average value is 62,30%).

The average value at all inhibition efficiency experiment temperatures is 74,21%.

The graphical representation of the inhibition percentage efficiency average values is notifying its decreasing with the temperature.

Time variation graphic of the inhibition efficiency at the experiment temperatures, have, relatively, a logarithmic form. The activation energy determined for the solution with HBTC, is with approx. 43% higher, than the activation energy from the solution without inhibitor, as for 86,07 KJ/mol compared with 60KJ/mol, revealing that the energy border for the corrosion reaction, rise in the presence of the inhibitor, and the corrosion reaction shall be rejected by the carbon steel surface spots, with high activation energy characteristics.

Analytical determined values for the activation energy are near graphical determined values, accordingly 59,41 KJ·mol⁻¹ and 85,43 KJ·mol⁻¹.

To study the HBTC molecules adsorption mechanism were calculated standard adsorption free energy values which are negative (spontaneous adsorption) very close with a chemisorption process. K values, determined in the same way, even high signifying an

intense adsorption, decrease with the rising of temperature from $1,799 \times 10^4$ at 25°C , to $0,496 \times 10^4$ at 55°C mean 3,62 times.

This might mean the (HBTC) inhibitor molecules adsorption intensity reduction at the surface of the carbon steel and developing of a desorption inhibitor process, at the surface of the carbon steel.

As well as the activation energy, the activation enthalpy, is increased in the inhibitor presence, meaning $82,45 \text{ KJ}\cdot\text{mol}^{-1}$ compared with $57,2 \text{ KJ}\cdot\text{mol}^{-1}$ proving an increasing of the energetical border for the corrosion reaction in presence of HBTC.

Potentiostatical method applied at the room temperature, finalised with the drawing of the polarity curves and Tafel segment extrapolation, had confirmed the corrosion inhibition effect of the carbon steel in HCl 2M solution in the presence of HBTC ($3,33 \times 10^{-4} \text{ M}$), proving that this one is a mixed inhibitor as well through displaying the potential values in both directions as through modifications of the Tafel slope segments. The corrosion current is reduced from $0,53 \text{ mA}/\text{cm}^2$ to $0,106 \text{ mA}/\text{cm}^2$, the percentage inhibition efficiency electrochemical determined being 80%.

This experimental sequence in which it was used HBTC compound at a single concentration, had proved the carbon steel inhibition corrosion effect in HCl 2M solution and emphasize the temperature influence over the developing of the processes, in the same solution of hydrochloric acid.

The carbon steel corrosion inhibition in HCl 2M, using as inhibitor APAS, in different concentrations

It was intended to investigate determined effects of different concentrations of APAS in HCl 2M solution over the carbon steel corrosion. It had been in mind the fact that the elements from APAS molecules which can favourise the adsorption of APAS molecules at the carbon steel surface, are relative identical with the one from HBTC molecules, and the molecular bigger mass (214 – APAS compared with 195 – HBTC) might be able, as well, to favourise the adsorption.

From the weight loss point of view, had been determined the corrosion rates (k_g) and penetration index I_p , also in HCl 2M solution without inhibitor as well in HCl 2M solution with APAS having the following concentrations : 0,1 mM; 0,2 mM; 0,3 mM; 0,4 mM.

APAS presence in HCl 2M solution, is determining the following decreaseings of the corrosion rate, ($\text{g}\cdot\text{m}^{-2}\cdot\text{h}^{-1}$) :

- at $c = 0,1 \text{ mM}$, reduction is 46%;
- at $c = 0,2 \text{ mM}$, reduction is 55%;
- at $c = 0,3 \text{ mM}$, reduction is 64%;
- at $c = 0,4 \text{ mM}$, reduction is 75%.

The same differences can be observed in the case of corrosion rate noticed as penetration of the corrosion. It is obvious the carbon steel corrosion rate decreasing effect obtained through increasing of APAS concentration and over the values of the percentage inhibition efficiency from weight loss (at $c = 0,4 \text{ mM}$, $P = 74,2\%$, and $P = 45,7\%$ at $c = 0,1 \text{ mM}$).

Carbon steel corrosion inhibition due to the presence of APAS in HCl 2M solution, is the result of the adsorption of APAS molecules at the metal surface, by the couple of sulphur

unparticipant electrons forming a link metal-sulphur and/or the adsorption of APAS on the carbon steel surface, by the nitrogen atom. It is possible to use the interpretation that it is formed a complex between the APAS molecules as ligand and different metallic atoms from the carbon steel net.

Adsorption is confirmed by the increased value of equilibrium constant (adsorption-desorption) $K = 6675,5 \text{ M}^{-1} \cdot \text{L}$ and by the free standard adsorption enthalpy

$\Delta G_{ads}^0 = -31,75 \text{ KJ} \cdot \text{mol}^{-1}$ which indicate a spontaneously adsorption process.

Adsorption isotherm which correspond to the experiment figures, is Langmuir isotherm. Carbon steel polarity curves for APAS investigated concentrations shows, compared with the obtained potentiostatically polarity curves in no APAS HCl 2M solution, that the APAS inhibitor is manifesting itself as a mixed inhibitor, but with main anodic action (strongly influencing the metal dissolving reaction). In the same respect, the electrochemical parameters values determined from Tafel straight lines confirm the fact that APAS is a mixed inhibitor with major anodic action.

The inhibition percentage efficiency electrochemical determined, is close in value to the weight loss one (at $c = 0,4 \text{ mM}$ APAS, $P_g = 74,2\%$ și $P_e = 76,5\%$).

The examination of the corroded samples in HCl 2M solution and in HCl 2M solution with APAS experimented concentrations through electronic microscopy reveals the formation of a thin film on the carbon steel surface.

Mössbauer spectroscopy indicate in the corroded samples case in HCl 2M solution with APAS, that the corrosion processes are considerably slowed down. As well the Mössbauer spectroscopy shows that a Fe superficial compound was formed without a magnetic arrangement on the sample surface. At this stage the principal corrosion product is a oxyhydroxide non-stoichiometrical amorphous of Fe^{3+} , consisting of a mixture of α , β și γ - FeOOH .

The Mössbauer parameters of the compound found on the corroded sample in the solution consisting inhibitor, is not significantly different compared to the corroded sample parameters in HCl 2M solution without inhibitor.

We consider that APAS inhibitor behaviour is like a "rust transformer" and is favouring formation of a "superficial closed layer". The inhibitor transform some constituents of rust into corrosion inhibiting oxide phases.